

AMENDMENTS TO THE CLAIMS

The following listing of claims will replace all prior versions of listings of claims.

In the Claims:

1. (Original) A polymer foam obtained by highly concentrated internal phase emulsion polymerization, which is formed from a crosslinked, exclusively hydrocarbon, polymer based on styrenic monomers and which exhibits a density at least equal to 6 mg/cm³ and at most equal to 20 mg/cm³ and cells with a mean diameter at most equal to 20 microns.
2. (Original) The polymer foam as claimed in claim 1, in which the polymer is a copolymer of styrene and of divinylbenzene.
3. (Original) The polymer foam as claimed in claim 2, in which the ratio by weight of the styrene to the divinylbenzene in the copolymer is between 4 and 1 and is preferably equal to 1.
4. (Currently Amended) The polymer foam as claimed in ~~any one of the preceding claims~~ claim 1, which exhibits a mean cell diameter of between 2 and 10 microns.
5. (Currently Amended) The polymer foam as claimed in ~~any one of the preceding claims~~ claim 1, in which the elements other than the constituent carbon and the constituent hydrogen of the polymer represent less than 3% by weight of the weight of the foam.
6. (Currently Amended) A process for the manufacture of a polymer foam as claimed in ~~any one of claims 1 to 5~~ claim 1, which comprises the following stages:
 - a) producing an emulsion between an organic phase comprising exclusively hydrocarbon styrenic monomers and sorbitan monooleate in ethylbenzene and an aqueous

phase comprising an electrolyte and sodium persulfate, the volume of the aqueous phase representing at least 96% of the total volume of the two phases;

- b) polymerizing said monomers until a solid foam is obtained;
- c) washing the foam obtained in stage b) and subjecting it to drying with supercritical CO₂.

7. The process as claimed in claim 6, in which the styrenic monomers present in the organic phase are styrene and divinylbenzene monomers.

8. The process as claimed in claim 7, in which the ratio by weight of the styrene monomers to the divinylbenzene monomers is between 4 and 1 and is preferably equal to 1.

9. (Currently Amended) The process as claimed in ~~any one of claims 6 to 8~~ claim 6, in which the styrenic monomers represent from 40 to 60% by weight of the weight of the organic phase.

10. (Currently Amended) The process as claimed in ~~any one of claims 6 to 9~~ claim 6, in which the sorbitan monooleate represents from 20 to 30% by weight of the weight of the organic phase.

11. (Currently Amended) The process as claimed in ~~any one of claims 6 to 10~~ claim 6, in which the electrolyte is aluminum sulfate.

12. (Currently Amended) The process as claimed in ~~any one of claims 6 to 11~~ claim 6, in which the electrolyte represents from 0.1 to 2% by weight of the weight of the aqueous phase.

13. (Currently Amended) The process as claimed in ~~any one of claims 6 to 12~~
claim 6, in which the sodium persulfate represents from 0.1 to 2% by weight of the weight of
the aqueous phase.

14. (Currently Amended) The process as claimed in ~~any one of claims 6 to 13~~
claim 6, in which the water present in the aqueous phase is ultrapure water.

15. The process as claimed in claim 14, in which the ultrapure water present in the
aqueous phase has a resistivity of approximately 16.2 megahms.

16. (Currently Amended) The process as claimed in ~~any one of claims 6 to 15~~
claim 6, in which the polymerization of the monomers is carried out at a temperature ranging
from 30 to 70°C.

17. (Currently Amended) The process as claimed in ~~any one of claims 6 to 16~~
claim 6, in which the washing of the foam comprises one or more washing operations with
water, followed by several washing operations with water/alcohol mixtures with an
increasing content of alcohol, themselves followed by one or more washing operations with
the alcohol.